

Water Balance And Management

by



Dr. D.D. BASU
Former Additional Director, CPCB
&
Advisor, CSE



What are the Consumption Pattern of Water in Industry?

- Make up for the Cooling Water system
- Make for Fire Water
- Feed to Demineralization Plant
- Process Water
- Service Water
- Sanitary Water

TYPICAL EXAMPLE OF WATER USAGE PATTERN

	1	2	3	4	5
Cooling water make-up (m ³ /day)	4800 (32.78)	690 (35.57)	2000 (55.04)	2223 (56.4)	21400 (35.91)
Feed to DM plant (m ³ /day)	4800 (32.78)	280 (14.43)	840 (23.12)	1080 (27.4)	11200 (18.79)
Process water (m ³ /day)	1200 (8.2)	290 (14.94)	271 (7.46)	271 (7)	15000 (25.17)
Service water (m ³ /day)	2400 (16.39)	300 (15.46)	523 (14.39)	250 (6.3)	7000 (11.74)
Sanitary water (m ³ /day)	1440 (9.84)	380 (19.58)	--	120 (2.9)	5000 (8.39)
Total (m ³ /day)	14640 (100)	1940 (100)	3634 (100)	3944 (100)	59600 (100)



What are the Sources of Waste Water in Industry?

- Cooling Tower Blow down.
- D.M. Plant regeneration Waste Water and Boiler Blow Down.
- Process Waste Water
- Service Water and Storm Water.
- Sanitary Waste Water.

TYPICAL EXAMPLE OF WASTEWATER GENERATION

S. No.		Petrochemicals complex	Phenol cumene plant	Caprolactum plant	Large petrochemical complex
1	Cooling tower blow-down	50	*	17	11200
2	DM plant regeneration wastewater	50	3	-	1400
3	Process wastewater	110	12	11	14000
4	Service wastewater	90	13	22	(See note 1)
5	Sanitary wastewater	40	8	-	2500
Total		340	36	50	29100

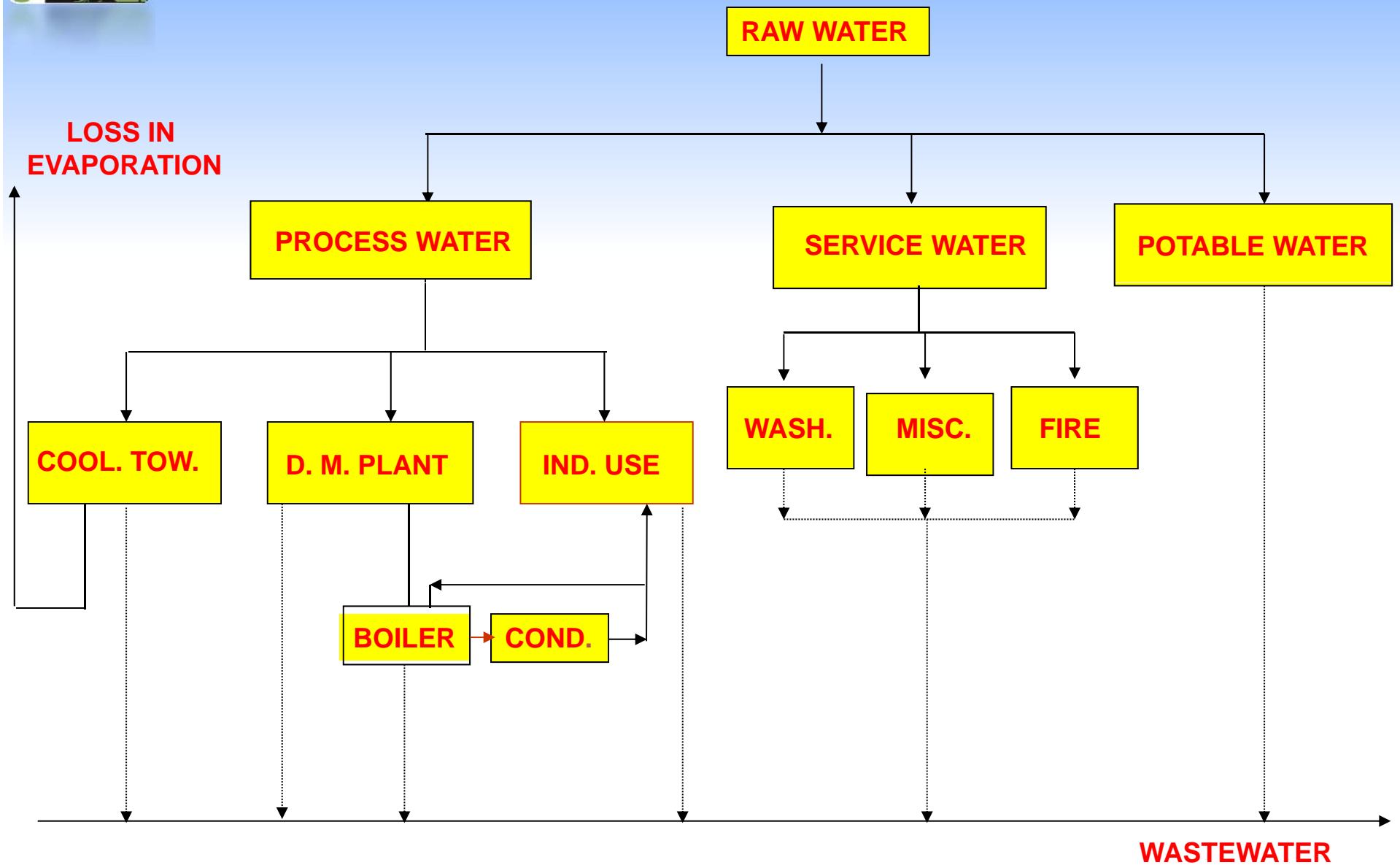
NOTE:

* - Industry claims insignificant blow-down.

1. Service wastewater quantity is included in the process wastewater



WATER BALANCE



Cooling Water Management

- Functions of Cooling Tower:-

Cooling Tower regulated temperature by dissipating heat from recirculating water used to cool chillers, air conditioning equipments or other process equipment. Heat is rejected primarily through evaporation. Therefore, by design cooling tower consumes significant amounts of water.

Factors for loss of water

- Evaporation – Major Source
- Drift – Water loss as a mist or small droplets
- Blow down or bleed off – control of concentration of total dissolved solids.
- Basin leaks or overflow – properly operated cooling tower should not have basin leaks or overflow. Good maintenance of system value and basin level control system is required.

The sum of water loss can be replaced by make up water

Make up water = Evaporation + Blow down + Drift

Concentration Ratio - The Key Parameter

A Key parameter used to evaluate cooling tower operations is concentration ratio.

$$\text{Concentration ratio} = \frac{\text{Concentration of TDS in Blowdown water}}{\text{Concentration of TDS in make up water}}$$

If Concentration ratio is high, water efficiency will be high but scaling, corrosion will be high.

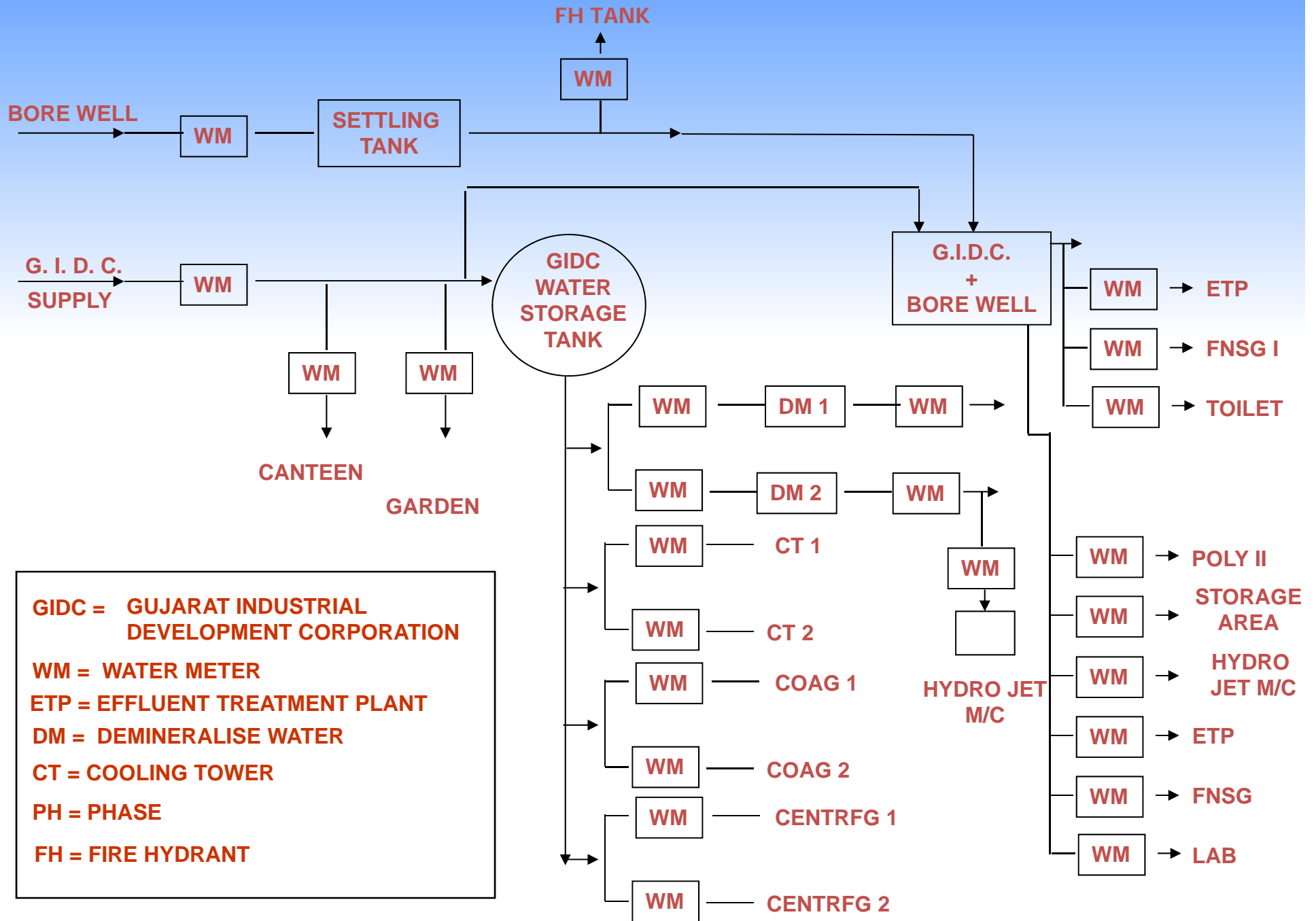
Water quality and Cycle of Concentration

Water Status	Conductivity	Total Hardness mg/l as CaCO_3	Calcium Hardness	Total Alkalinity	PH
Makeup water	600	300	150	200	7.5
2 coc	1200	600	300	400	8.0
4 coc	2400	1200	600	800	8.5
6 coc	3600	1800	900	1200	6.6
10 coc	6000	3000	1800	2000	9.0

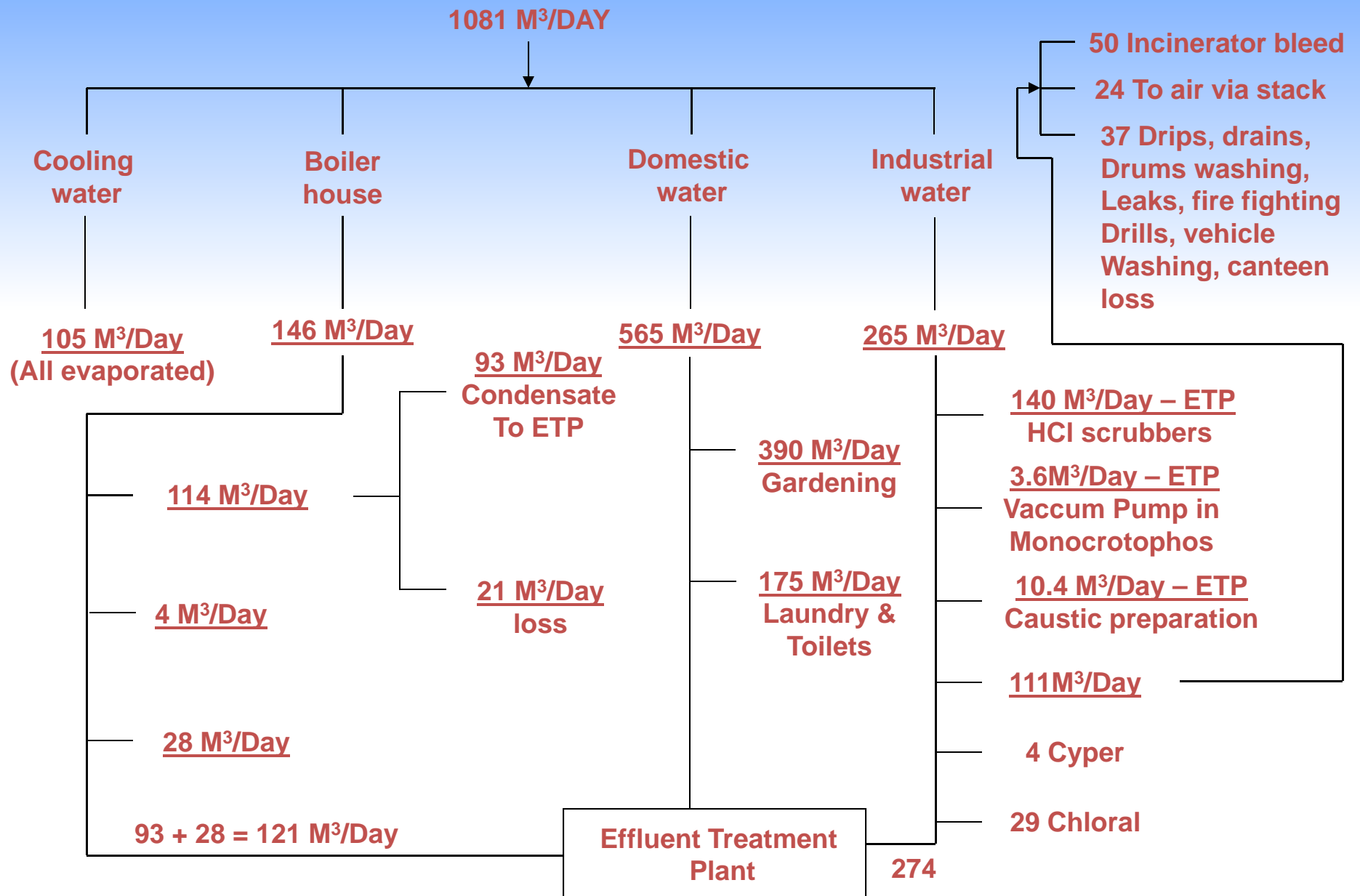
This Indicates 4 to 6 cycle shall be the ideal coc for cooling tower recirculation source guidelines managing water cooling system for owners, operators, environmental managers

SAN JOSE / SANTA CLARA Water pollution control Plants

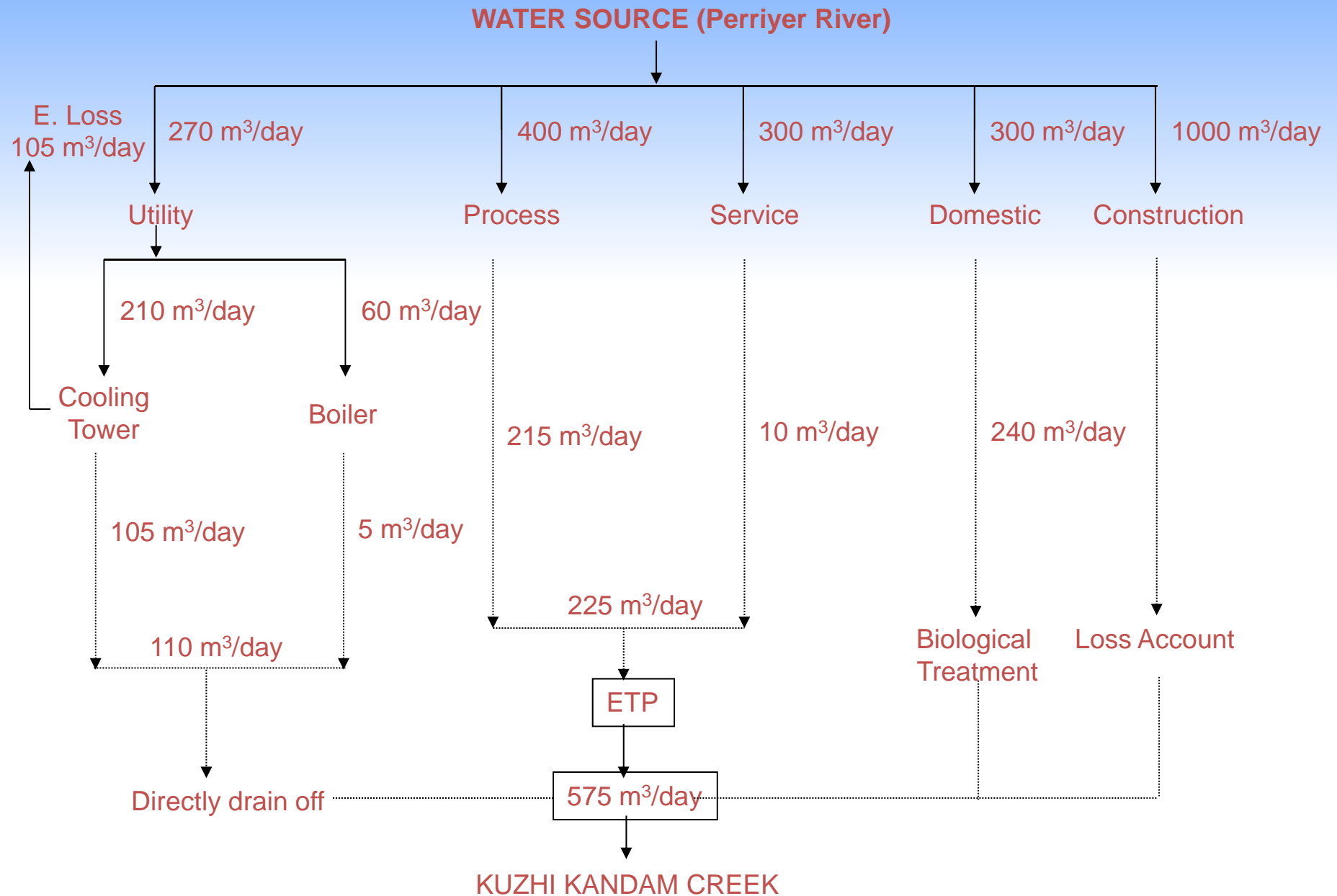
WATER DISTRIBUTION NETWORK



WATER BALANCE IN MONOCROTOPHOS PLANT



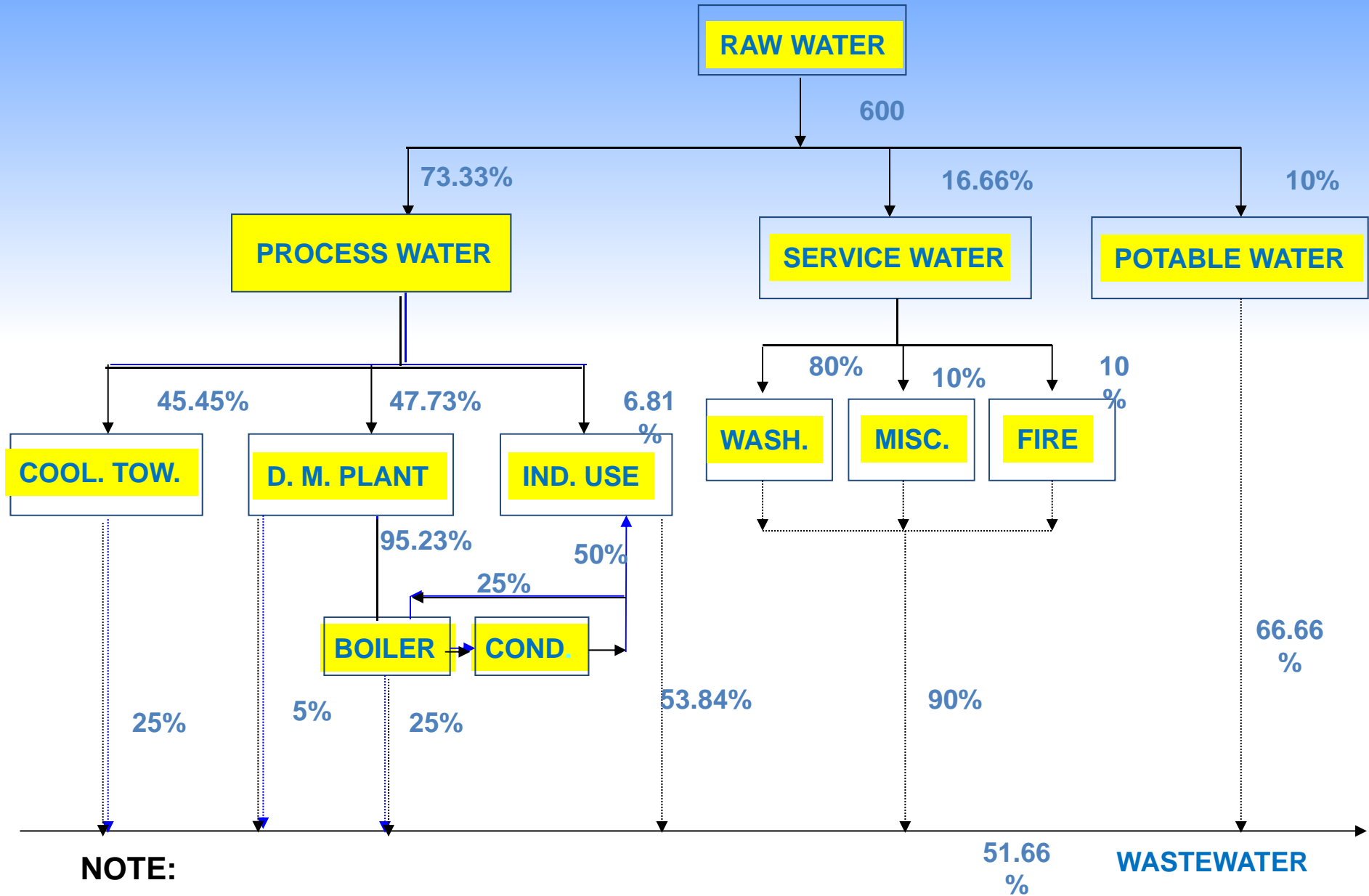
WATER BALANCE IN HIL PLANT



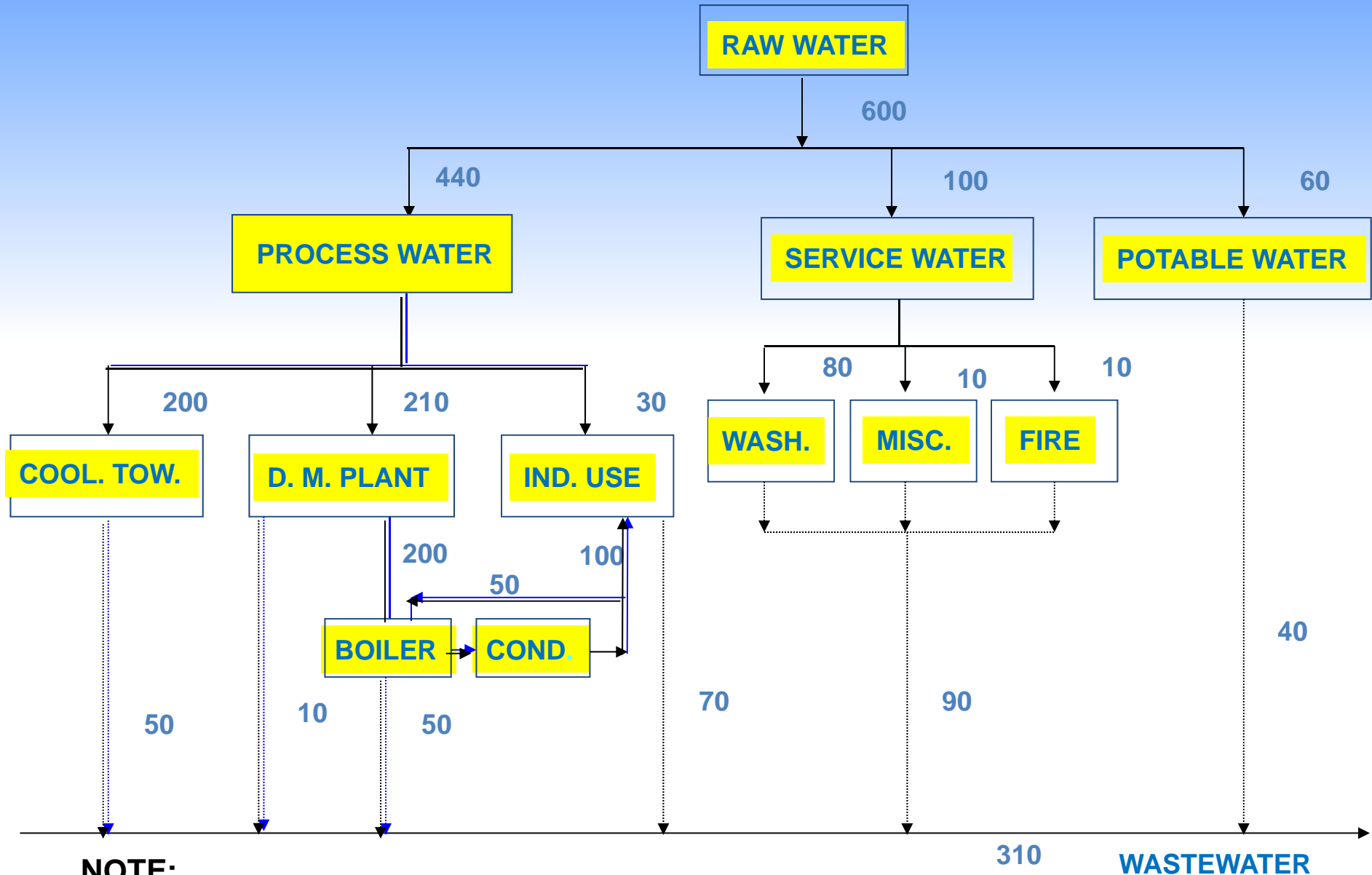


Thumb Rule for Water Balance

MASS BALANCE OF WATER CONSUMPTION AND EFFLUENT GENERATION



MASS BALANCE OF WATER CONSUMPTION AND EFFLUENT GENERATION





4 R – Concept

- RENOVATION
- RECYCLING
- REUSE
- RECHARGE



Step by Step Approach on 4R – Concept

- Waste water characterization
- Inter-relationship of solids
- Chemical characterization of total solids
- Approach to develop
Renovation/Recycling/Reuse/Recovery



WASTEWATER CHARACTERISATION



WASTE WATER CHARACTERIZATION

Total solid (TS)

Residue after evaporation and dried at 103° - 105° C

Total volatile solids (TVS)

Those solids which are burnt off or volatilized when the TS are ignited

$$\text{TVS} = \text{TS} - \text{TFS}$$

Total fixed solids (TFS)

Residue that remains after TS is ignited [500 ± 50°C]

(Portion of TS retained at filter paper and dried at 105°C)

Total suspended solids (TSS)

Volatile Suspended Solids (VSS)

TSS when burnt off at 500° ± 50°C

$$\text{VSS} = \text{TSS} - \text{FSS}$$

Fixed Suspended Solids (FSS)

Residue remains when TSS are ignited [500° ± 50°C]

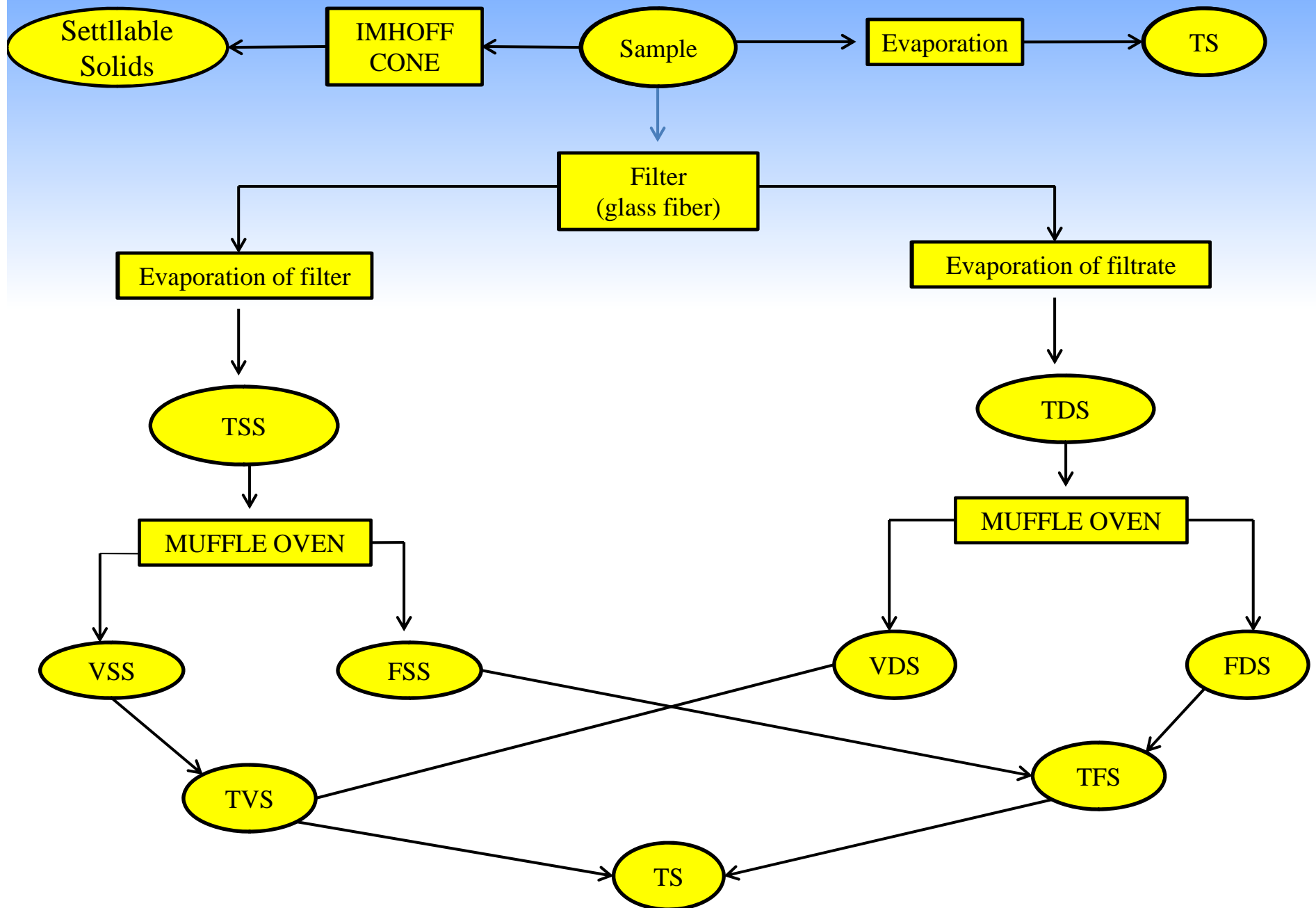
Total dissolved solids (TDS)

Total Volatile dissolved solids VDS (burnt off at 500° ± 50°C)

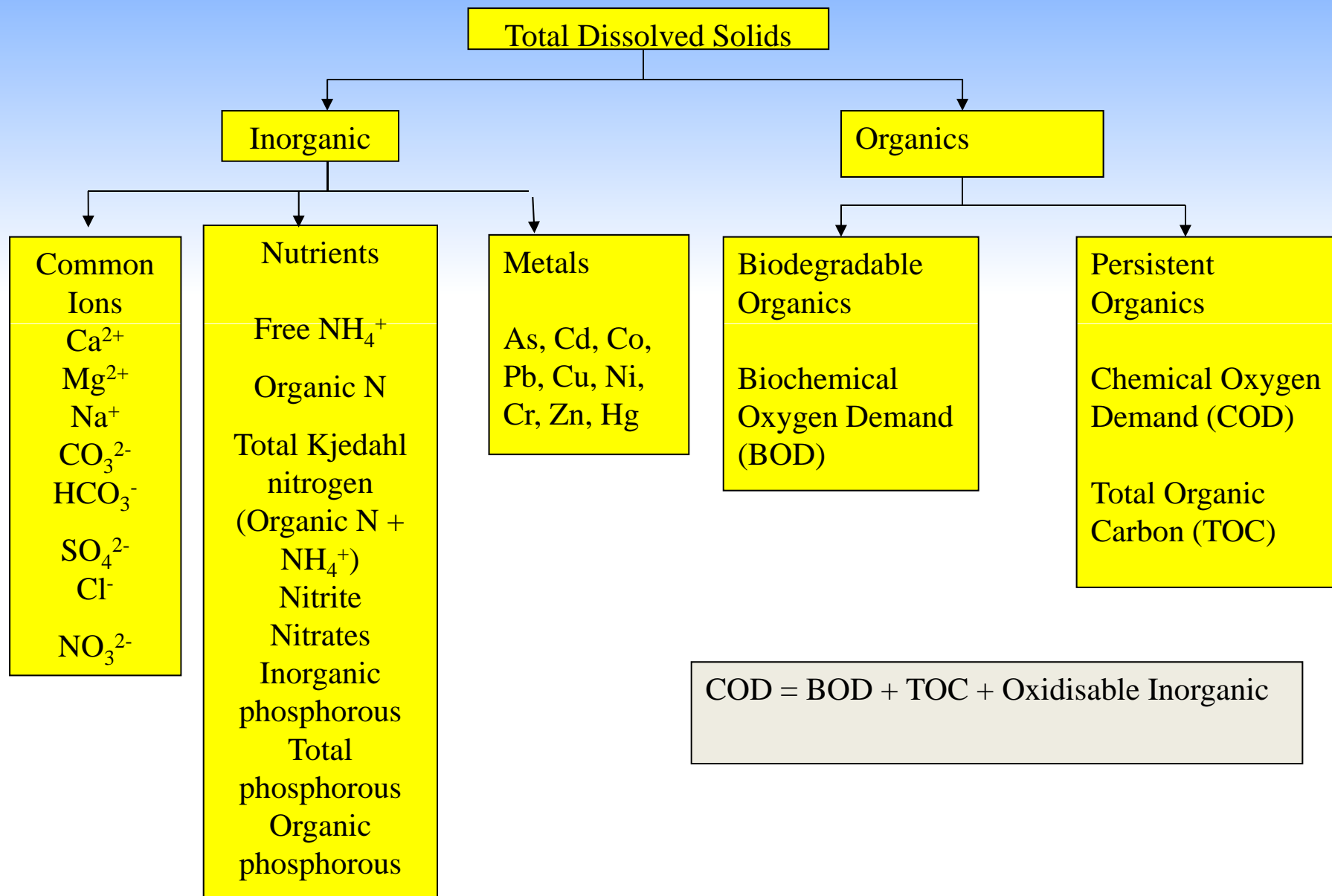
Fixed Dissolved Solids (FDS)
Residue remains when TDS is ignited at [500° ± 50°C]

$$\text{TDS} = \text{TS} - \text{TSS}$$

INTER RELATIONSHIP OF SOLIDS

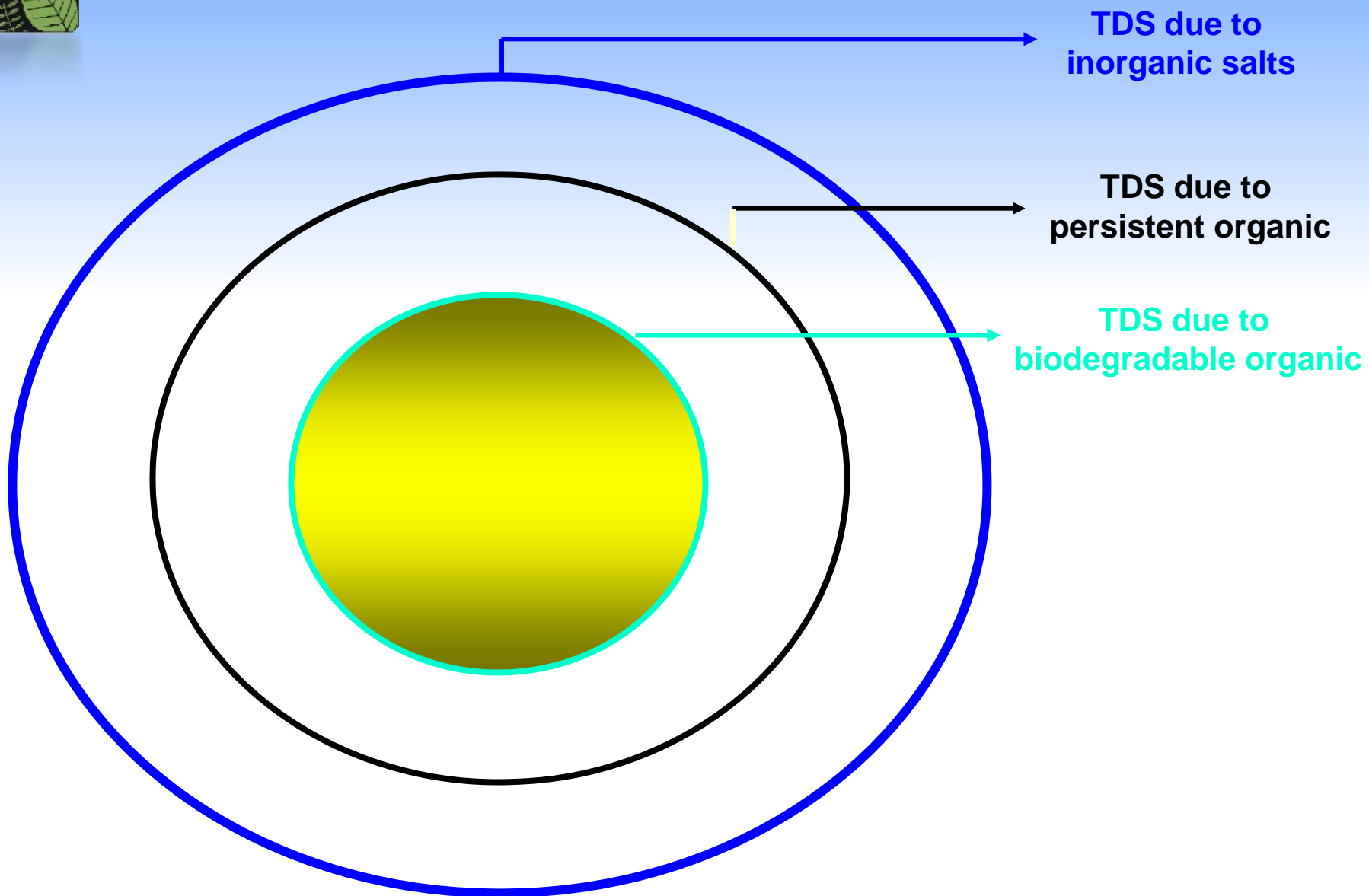


CHEMICAL CHARACTERIZATION OF TOTAL DISSOLVED SOLIDS





TDS / BOD / COD RELATIONSHIP



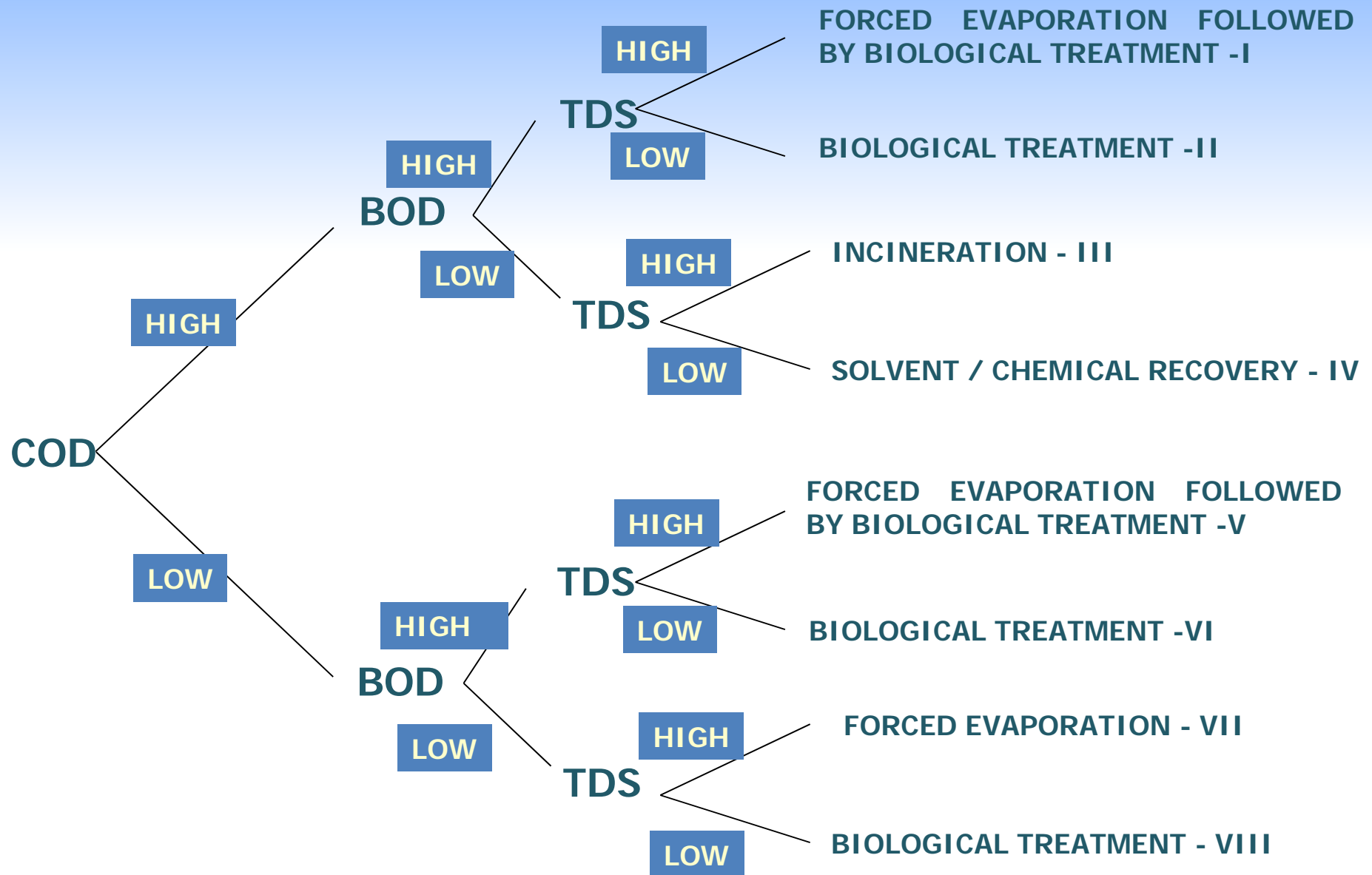


Approach to develop Renovation/Recycling/Reuse/Recovery

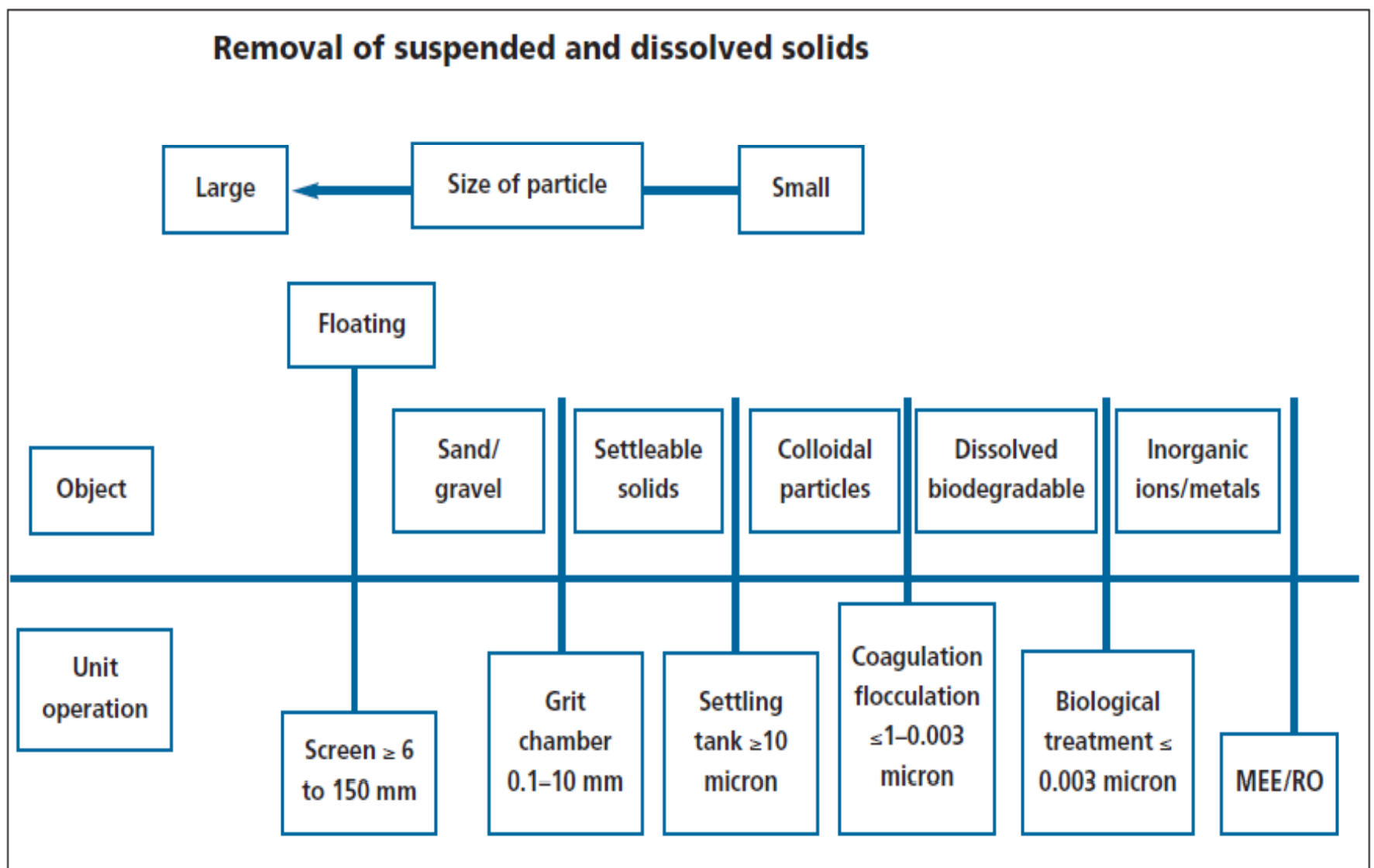
- In plant control
- Treatment option
- Segregation of streams
- ISBL and OSBL

SEGREGATION OF STREAMS

STREAMWISE BEST PRACTICABLE TECHNOLOGY IN CHEMICAL INDUSTRIES

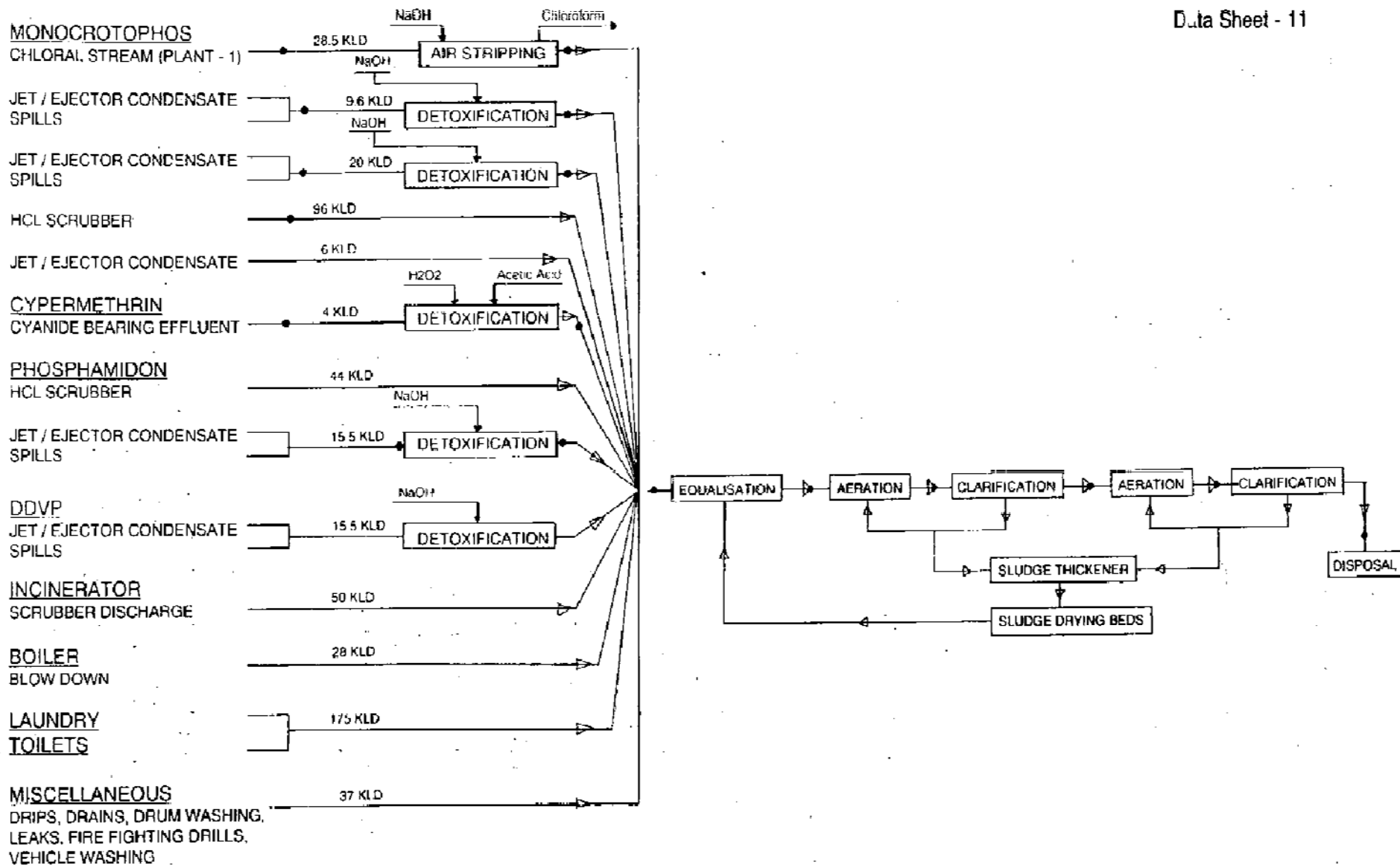


OSBL Treatment

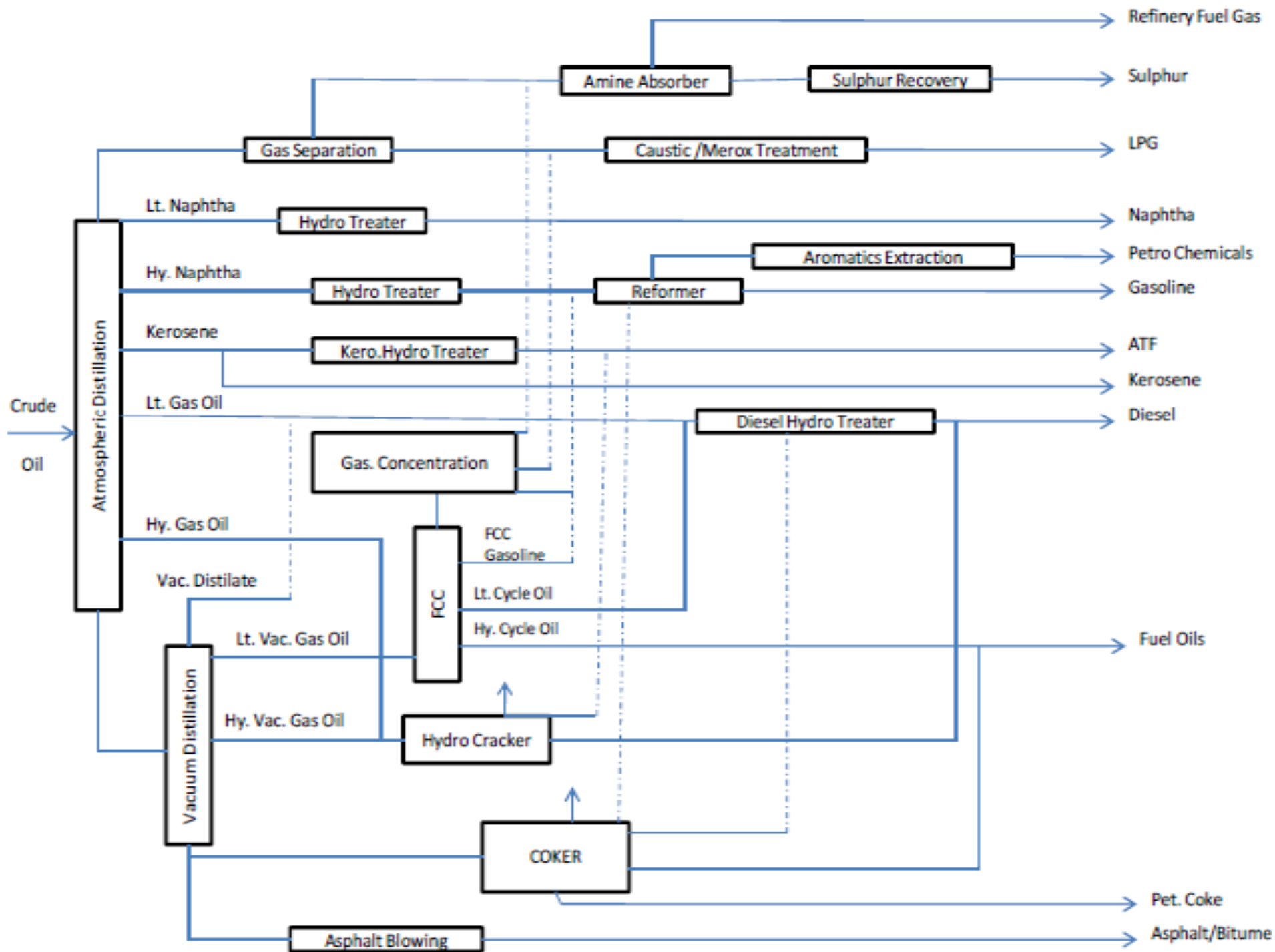


INTEGRETED WASTEWATER SYSTEM (ISBL & OSBL)

Data Sheet - 11



(DDVP OR PHOSPHAMIDON ARE IN PRODUCTION ONLY ONE AT A TIME)



➤ Representative Concentrations of Pollutants in Typical Refinery Effluents

	Oil	H ₂ S (RSH)	NH ₃ (NH ₄ ⁺)	Phenols	BOD COD TOC	CN- (CNS-)	TSS
Distillation Units	XX	XX	XX	X	XX	-	XX
Hydrotreatment	XX	XX(X)	XX(X)	--	XX	--	--
Visbreaking	XX	XX	XX	XX	XX	X	X
Catalytic Cracking	XX	XXX	XXX	XX	XX	X	X
Hydrocracking	XX	XXX	XXX	--	X	-	-
Lube Oil	XX	X	X	-	XX	-	-
Spent Caustic	XX	XX	-	XXX	XXX	X	X
Ballast Water	X	-	-	X	X	X	X
Utilities (Rain)	-(X)	-	-	-	X	-	-
Sanitary/Domestic	-	-	X	-	X	-	XX

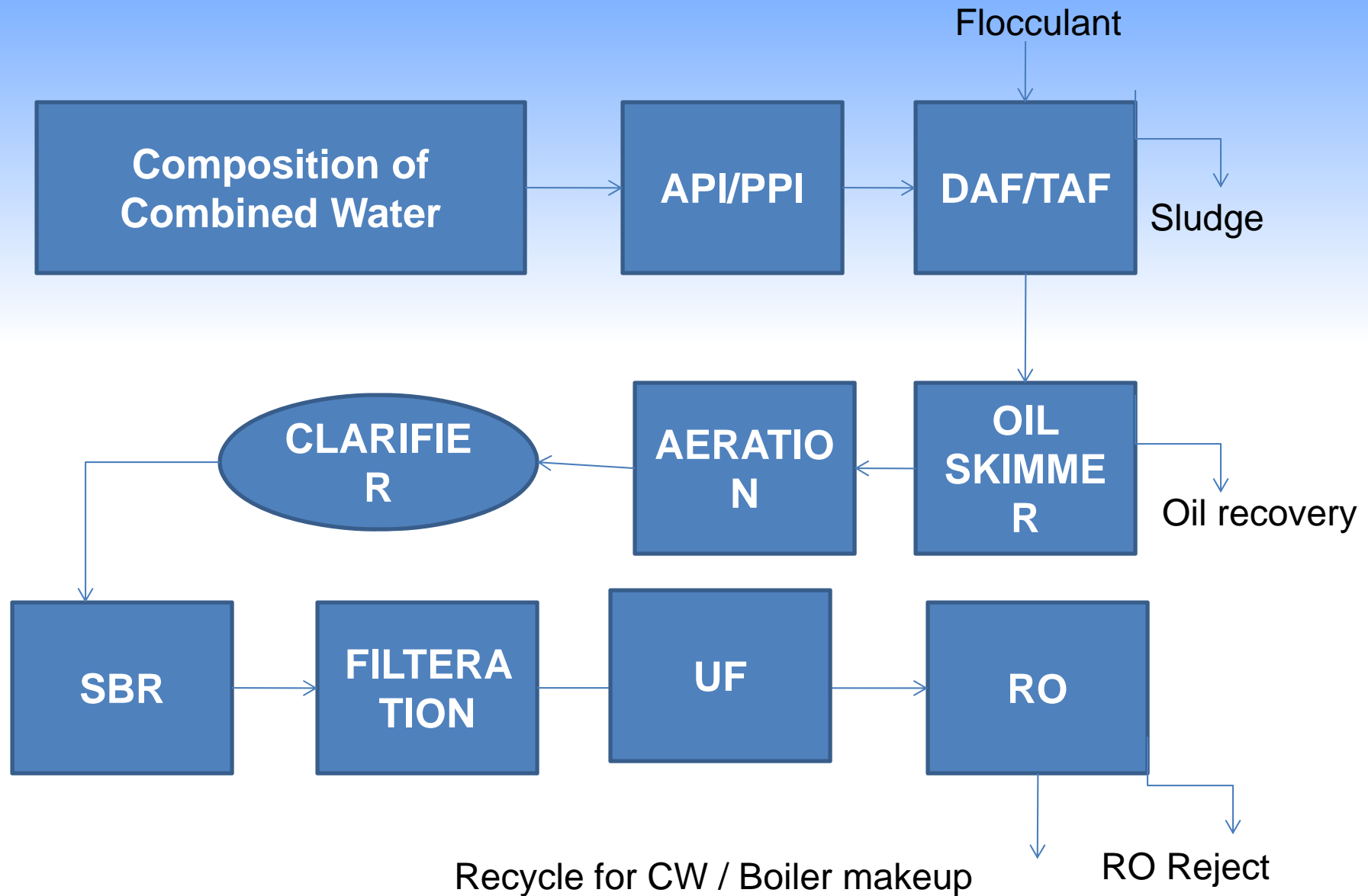
Key: X=<50 mg/l; XX=50-500 mg/l; XXX=>500 mg/l

ISBL

UNIT OPERATION	FLOW (L/TON)	IN-SITU TREATMENT
Desalter	30-100	CPI
ADU+VDU	26	CPI/ Stripping
VC/TC	56	CPI/ Stripping
Cooking	25	Stripping
Catalytic cracking	60-90	Stripping
Catalytic Hydrocracking	26	Stripping
Alkylolation		
Isomerisation		
Catalytic Refining		
Gas Treatment		
Dewaxing/solvent		Solvent recovery
Heat exchanger		
Blow down		CPI



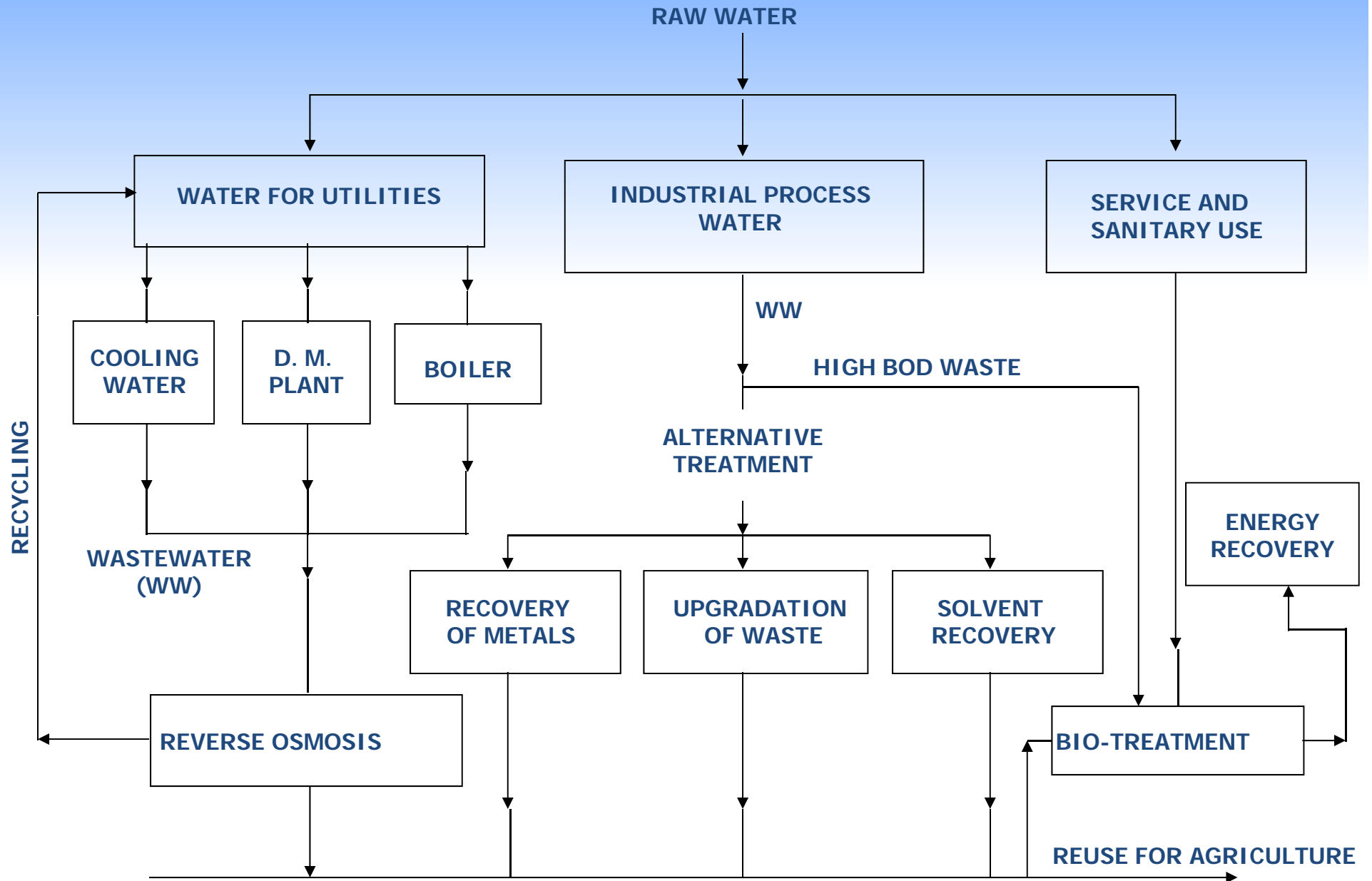
OSBL





Treated Effluent Option of Renovation, Recycling and Reuse.

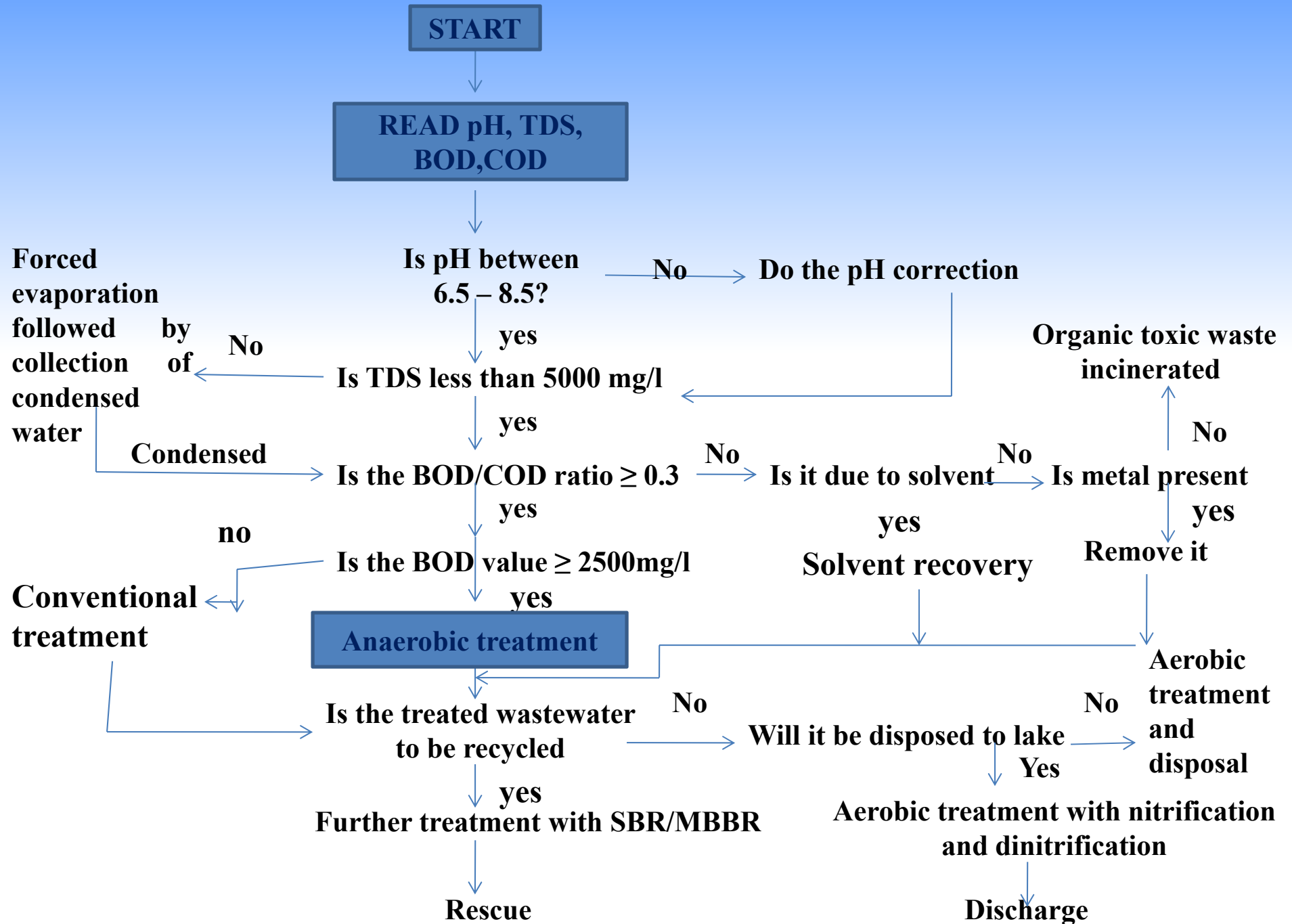
POSSIBLE OPTIONS OF RENOVATION, RECYCLING AND REUSE OF WASTEWATER



Best Management System

- Reuse of condensate water which has low minerals content and typically is generated in good amount when cooling tower load is high.
- Reuse and Recycle of treated effluent after appropriated treatment.
- Use softening plant to reduce total dissolved solids in makeup water.
- Use Treated Sewage as makeup water
- Install real time conductivity measurement to both raw water, makeup and blowdown water.
- Check and maintenance basin leaks or overflow
- Avoid ground water source as cooling tower makeup.

HOW TO CHOOSE INDUSTRIAL WASTEWATER TREATMENT SCHEME



What will be the appropriate treatment?

Problem no 1

If pH -5.5, BOD – 3000mg/l, COD – 5000 mg/l,
BOD-COD ratio – 0.6, SS – 100 mg/l

Problem no 2

If pH -6.5, BOD – 600mg/l, COD – 1000 mg/l,
BOD-COD ratio – 0.6, SS – 200 mg/l

Problem no 3

If pH -7.5, BOD – 1000mg/l, oil and grease – 100mg/l,
COD – 3000 mg/l, SS – 200 mg/l

Problem no 4

If pH -8.00, BOD – 200mg/l, COD – 3000 mg/l

Problem no 5

If pH -6.5 -8.5, BOD – 250mg/l, COD – 500 mg/l,
SS – 150 mg/l.

If you Salute your Duty,
You no need to Salute
Anybody,
But
If you pollute your
Duty, You have to
Salute Everybody
-Kalam

For more Quotes:





THANK YOU!